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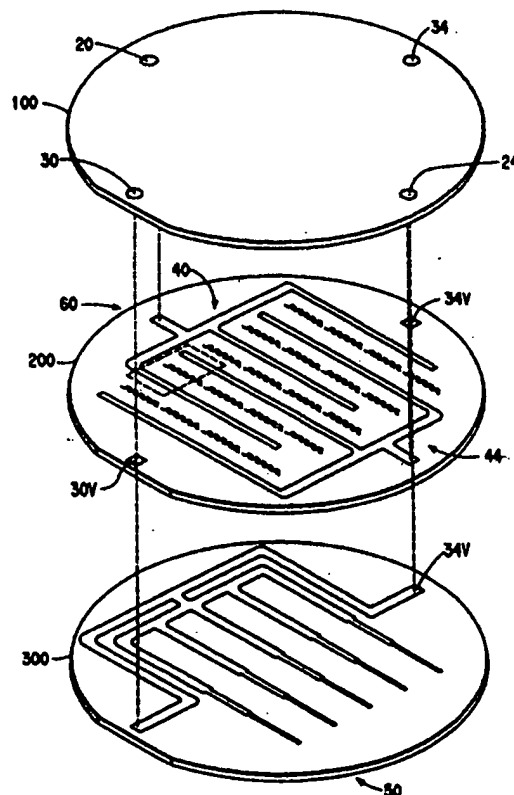
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(54) Title: CHEMICAL MIXING AND REACTION APPARATUS AND PROCESSES FOR THE PREPARATION THEREOF

(57) Abstract

An integral structure is provided for chemical processing, particularly high-speed mixing and chemical reacting, in which a plurality of laminae (100, 200, 300) are joined together and having inlet (20, 24) and outlet ports (30, 34) connected by a plurality of intersecting channels formed therethrough which accommodate the passage of one or more chemicals, said laminae (100, 200, 300) comprising a material selected for compatibility with the one or more chemicals, the channels being formed so that chemicals are combined at intersections therein at sufficient angles of attack and shear rates so that chemical reactions are not limited by mass transfer. Chemicals are introduced through the inlet ports (29, 24) and processed along the channel, with desirable product withdrawn through the outlet ports (30, 34). The laminae are selected from material of groups III, IV or V of the Periodic Table. Processes of manufacture of the apparatus and processes utilizing the apparatus are also disclosed herein.



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TITLE OF THE INVENTION  
CHEMICAL MIXING AND REACTION APPARATUS  
AND PROCESSES FOR THE PREPARATION THEREOF  
FIELD OF THE INVENTION

5        This invention relates to an integrated chemical processing apparatus, adapted for use with high-speed chemical reactions, which can be incorporated into a larger integral structure of multiple chemical processing units or an integrated system. More  
10 particularly, the present invention is directed to chemical processing apparatus characterized by improved rapid mixing of chemicals passing therethrough, by enhanced safety of operation, and by reduced capital investment.

15        BACKGROUND OF THE INVENTION

To achieve efficient chemical processing, it is necessary to precisely control a number of processing parameters, such as temperature, pressure, mixing conditions, exposure of reactants to catalyst material,  
20 exposure of reactants to products and/or byproducts and exposure of reactants to actinic radiation. Certain chemical reactions are particularly difficult to perform in an optimal manner because the chemical reactions occur very quickly, sometimes before the reactants are  
25 completely mixed together. Certain non-stoichiometric portions of the partially mixed reactants may cause reaction products other than those desired to be produced.

Conventional chemical processing equipment  
30 typically holds a relatively large volume of materials and consequently has a relatively large volume to surface area ratio, and are thus particularly ill-suited for high speed chemical reactions. Different portions of the reactant materials contained within such  
35 processing equipment are more likely to be exposed to

different histories of conditions. In the case of a conventional tank reactor, for example, when reactants are introduced they are typically added in separate streams, usually at controlled rates, and are then mixed together. The so-called T-mixer has been used to mix incoming streams together before they enter a reactor tank. For chemical reactions that occur rapidly, i.e., typically in less than one second, insufficient mixing may have occurred, even with use of the T-mixer, before the reaction is well established. Portions of the incompletely mixed mixture may be starved of one or the other reactant and undesired secondary reactions may occur which produce undesired byproducts.

Rapid stirring of the reactants may reduce this mixing history difference, but will not eliminate it. As a result of the nonhomogeneous mixing history, different portions of the reactants may chemically react differently. Undesired reactions may occur in portions of the reactants that cause localized heating in these different portions. This localized heating may accelerate undesired reactions. This may result in the production of undesired waste products, which may be hazardous and/or which must be properly disposed of. In extreme situations, reaction rates may accelerate to uncontrollable levels, which may cause safety hazards, such as potential explosions.

If, however, the volume in each reactant stream being mixed is substantially reduced, then the speed of mixing of the reactants may be greatly increased to substantially improve the control of homogeneity of mixing history of the reactants.

It has been recognized that a high degree of flow turbulence enhances the ability to rapidly mix two or more reactants together. Rapid mixing is known to be important for rapid chemical reactions. A high degree

of turbulence is also known to enhance heat transfer as well as mixing rates. Thus a structure having both a low contained volume and a high degree of flow turbulence is particularly advantageous for precise control of high-speed chemical reactions.

Mixer assemblies having highly turbulent flow have been constructed by machining the desired passages and chambers in metal plates, using conventional metalworking techniques, and then assembling the plates into a stack and either clamping the stack together or permanently joining the stack, as by welding or soldering. An example is U.S. Patent 3,701,619. Structures formed using conventional machine tool techniques cannot economically achieve volume to surface area ratios that are very low. The materials of construction of conventional chemical processing apparatus, such as steel and specialty iron alloys, furthermore may be subject to corrosion and wear, may have undesirable effects on catalytic activity, or may "poison" a catalyst.

It is an object of the present invention to provide a chemical processing unit that mixes reactants in a rapid and efficient manner, such that chemical reactions are not limited by mass transfer considerations. The present invention provides the capability to integrate one or more mixing/reaction units with control elements into a larger integrated chemical processing system to meet the needs of a specific high-speed chemical reaction. A feature of the present invention is that it can be economically used in the laboratory, to make a range of precise sizes of mixing/reaction units, to perform the basic chemical reactions for determining the optimum operating parameters. Commercial production volumes may then be readily achieved by replicating the

mixing/r action units and operating them in parallel in a larger integrated chemical processing system.

Advantages of the present invention, when used in a larger integrated chemical processing apparatus, include the elimination of many interconnections and joints, thereby reducing the potential for leaks. These and other objects, features and advantages will become better understood upon having reference to the following description of the invention.

10 SUMMARY OF THE INVENTION

There is disclosed and claimed herein an apparatus for use in an integral structure for chemical mixing and reacting of one or more chemicals, comprising a plurality of laminae joined together and having a plurality of intersecting channels formed therethrough which accommodate the passage of one or more chemicals. The laminae comprise a material selected for compatibility with the one or more chemicals, the channels being formed so that chemicals are combined at intersections therein at sufficient angles of attack and shear rates so that chemical reactions are not limited by mass transfer considerations. Moreover, the shear rate is sufficient to disrupt boundary layer formation. The channels are arranged such that two or more channels are positioned at a point of intersection to form an angle of attack of from 20 to 160 degrees, preferably from 70 to 110 degrees, and most preferably about 90 degrees.

The apparatus of the invention may be prepared according to the process of the invention. The process comprises first, processing a plurality of laminae each having a top portion and a bottom portion and a desired thickness, sufficient to form desired pathways thereon or therethrough. The laminae are then stacked and

bonded together in precise alignment to develop channels that intersect at a desired angle of attack.

In the process for preparing the integral structure, the pathways on facing surfaces of adjacent laminae generally form passages through the structure in the plane of the laminae having the desired cross-sectional areas. These planar passages are connected with each other and with passages orthogonal to the plane of the laminae which pass through one or more laminae to form passages having the desired overall three-dimensional shapes.

The apparatus of the present invention may be used in a method for mixing and reacting of chemicals. The method comprises: (a) introducing one or more chemicals into channels of the above-described structure; (b) directing the chemicals to traverse the channels; (c) coordinating traversal at a traversal rate so that angles of attack and shear rates are sufficient to insure that chemical reactions are not limited by mass transfer considerations; and (d) withdrawing reacted product from the channels of the structure.

The invention can be more fully understood from the following detailed description thereof in connection with accompanying drawings.

#### BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 is a perspective view of an apparatus of the present invention.

Figure 2 is an exploded perspective view of the apparatus, as seen from above, showing the top surfaces of three laminae which are used to form the structure.

Figure 3 is an exploded perspective view of the apparatus, as seen from below, showing the bottom surfaces of three laminae which are used to form the structure.

Figure 4 is an enlarged first sectional view, taken along section lines 4-4 of Figure 1.

Figure 5 is an enlarged second sectional view, taken along section lines 5-5 of Figure 1.

5        Figure 6 is an exploded perspective view of a portion of the apparatus of Figure 1, showing the bottom surface of a first lamina 100 and the top surface of the second lamina 200. Figures 6, 8, 9 show a first  
10        embodiment arrangement of channels that form an array of mixing elements and a distribution manifold.

Figure 7 is an exploded perspective view of the bottom of a second lamina 200 and the top of a third lamina 300 showing channels that form a distribution manifold.

15        Figure 8 is an enlarged view of the portion of Figure 6 designated as 8-8 showing mixing element 64A2.

Figure 9 is an enlarged view of a portion of Figure 8 designated as 9-9.

20        Figure 10, which corresponds in scale to Figure 9, shows a second embodiment arrangement of channels that form an array of mixing elements and a distribution manifold.

25        Figure 11 is a simplified perspective view which illustrates the channels of Figure 8 and the intersections of those channels.

Figure 12 is a simplified perspective view which illustrates the channels of Figure 10 and the intersections of those channels.

30        Figure 13a-c is a plan view of the channels of Figure 9 showing the channels separately and superimposed.

#### DETAILED DESCRIPTION OF THE INVENTION

The present invention is characterized by small channels of complex three-dimensional shapes which:

35        (1) can create a high degree of flow turbulence that

enhance rapid mixing and heat transfer; (2) intersect with other channels in a shearing fashion at a predetermined angle of attack; (3) have a very low volume to surface area ratio that minimizes temperature gradients and further enhances heat transfer; and (4) controls residence time of materials therein, to achieve more precise temperature control, and a more uniform temperature history, for every portion of the entire volume of reactants mixed and reacted. Channels small enough that they will not allow the propagation of a flame may be readily formed and thus can be used to safely react potentially explosive chemical reactants. The channels may measure as small as about 10 micrometers in cross section.

Throughout the following detailed description, reference characters between 1 and 99 refer to overall features of the invention. That is, these features may only be apparent on joinder of adjacent laminae. For example, in Figure 7 chamber 50M is comprised of chamber 250M on laminae 200 and chamber 350M on laminae 300. Laminae are numbered 100, 200, 300, and specific features on each respective lamina are numbered 101 to 199, 201 to 299, etc. with the last two digits corresponding to the overall feature of the invention. The suffix letter "V" is used to designate interlamina vertical pathways, also known as "vias", through the structure. Similarly, suffix "M" indicates a manifold chamber within a manifold; suffixes "S" and "T" indicate straight and turning portions of pathways. Suffixes comprising a hyphen and numeral (-1, -2, etc.) are used to designate parts of specific elements, such as individual branches of the branched manifolds. A capital letter and number are appended to the reference character to designate elements of an array (e.g., mixer 64A2 of array 64). Numerals enclosed in curved braces

( ) designat crystal planes in a crystalline material (e.g., {100}).

Referring to Figure 1, there is shown an apparatus 10 exemplary of the present invention. This apparatus 10 is comprised of a plurality of laminae 100, 200, 300 fused together to form an integral structure. One or more inlet ports (here, inlet ports 20 and 24 are shown) enable the flow of reactants into the apparatus and one or more outlet ports (here, outlet ports 30 and 34 are shown) enable the flow of the resulting reaction products out of the apparatus. It is to be appreciated that the inlet ports 20 and 24 and outlet ports 30 and 34 do not necessarily have to be positioned only through lamina 100 as shown but may extend through all three laminae (e.g., outlet port 34 in Figure 4). These elements could be arranged to meet the integral structure at the side of a lamina, for example (not shown). The laminae may be comprised of either the same or different materials. The laminae (also known as wafers) 100, 200, 300 preferably are comprised of materials from groups III, IV or V of the Periodic Table, silicon being the most preferred material. If desired one or more of the laminae may be comprised of an alternate material, such as ceramic, a glass material such as Pyrex or other compatible materials.

Figure 2 shows the top surfaces of the three laminae 100, 200, 300 and Figure 3 shows the bottom surfaces of the three laminae 100, 200, 300 which are used to form the apparatus of Figure 1. Operative features of the apparatus shown in Figures 2 and 3 are: two inlet distribution manifolds 40, 44 formed by pathways in the bottom surface of lamina 100 and the top surface of lamina 200; an array 60 of mixer/reaction chambers represented by a series/parallel arrangement of T-mixers 62 and intersecting-channel mixing elements 64

formed by corresponding pathways in the bottom surface of lamina 100 and the top surface of lamina 200; a fork-shaped outlet collection manifold 50 formed by corresponding pathways in the bottom surface of lamina 200 and the top surface of lamina 300.

In sectional views of Figures 4 and 5 the vertical scale is exaggerated for clarity of illustration. Although the laminae of the apparatus are fused into an integral structure when completely fabricated, for clarity of illustration the interfaces between the laminae are shown in Figures 4 and 5.

In Figures 4 and 5, which illustrate typical flow passages in the interior of the structure, the vertical pathways 20V, 24V, 30V, 34V which connect respectively with the inlet ports 20, 24 and outlet port 30 in lamina 100 and outlet port 34 in outer laminae 100 and 300, are typically formed by grinding or drilling through the lamina.

In Figure 4 three passages 40-1, 40-2, 40-3, which are branches of distribution manifold 40 and three passages 44-1, 44-2, 44-3, which are branches of distribution manifold 44 are formed in the top surface of lamina 200. Five passages 50-1, 50-2, 50-3, 50-4, 50-5, which are branches of collection manifold 50, are respectively formed by corresponding mirror image pathways 250-1, 250-2, 250-3, 250-4, 250-5 (see also Figure 7) in the bottom surface of lamina 200 and pathways 350-1, 350-2, 350-3, 350-4, 350-5 (Figure 7) in the top surface of lamina 300.

In Figure 5 the central axis of a third horizontal passage 50-3 (see also Figure 8), which comprises the center branch of a 5-branch collection manifold 50, lies in the plane of the sectional view. The horizontal passage 50-3 is formed by corresponding mirror image pathways, respectively pathway 250-3 (Figure 7) in the

bottom surface of lamina 200 and pathway 350-3 (Figure 7) in the top surface of lamina 300. The passages which comprise the 5-branch collection manifold 50 in the exemplary apparatus are formed using an etching technique.

In Figure 5 passages 160A, 160B, 160C, 160D, in combination with the branches 40-1, 44-1; 44-1, 40-2; 40-2, 44-2; and 40-3, 44-3 of distribution manifolds 40, 44 (Figures 4 and 7) form an array of T-mixer structures 62 whose operation will be subsequently described in conjunction with Figures 6, 7. The passages 164 in the bottom surface of the lamina 100 and the passages 264 in the top surface of lamina 200 cooperate to form an array of mixing chambers 64, each of which comprises a plurality of intersecting channels (Figure 6).

At the left of Figure 5 is vertical passage 20V, which extends through lamina 100 to connect inlet port 20 with the common chamber 40M of manifold 40. At the right of Figure 5 is vertical passage 24V, which extends through lamina 100 to connect inlet port 24 with common chamber 44M of manifold 44. A third branch 50-3 of 5-branch manifold 50 is formed by corresponding mirror image pathways 250-3 and 350-3 (Figure 7) in the bottom surface of lamina 200 and the top surface of lamina 300, respectively. Mixing chambers 64A3, 64B3, 64C3, 64D3 are visible in Figure 5.

Figure 6 shows an arrangement of pathways that cooperate to form an array of mixer/reaction chambers 60 and a pair of distribution manifolds 40, 44. First distribution manifold 40 is comprised of common chamber 40M and branch passages 40-1, 40-2, 40-3. The chamber 40M is formed by the combination of chamber 140M, on the bottom surface of the first lamina 100, and chamber 240M on the top of lamina 200. Also shown is the opening of

vertical pathway 20V which connects input port 20 with the common chamber 40M.

S cond distribution manifold 44 is comprised of common chamber 44M and branch passages 44-1, 44-2, 44-3.

5 The chamber 44M is formed by the combination of chamber 144M, on the bottom surface of the first lamina 200, and chamber 244M on the top of lamina 200. Also shown is the opening of vertical pathway 24V which connects input port 24 with the common chamber 44M.

10 A series of serpentine pathways 164 are formed on the bottom surface of the first lamina 100, which cooperate with corresponding serpentine pathways 264 of lamina 200, to form the array of intersecting-channel mixing elements 64 (here, 64A5 formed from 164A5 and  
15 264A5 in Figure 6) of the mixer array 60. The mixer array 60 comprises multiple groups 60A (e.g., 64A1-64A5), 60B, 60C, 60D of multiple parallel mixers 64. In the specific example shown, there are five mixers in each group, that are respectively designated  
20 64A1, 64A2, 64A3, 64A4, 64A5 through 64D1, 64D2, 64D3, 64D4, 64D5. Figure 6 also shows chambers 40M and 44M, previously mentioned.

Each mixer 64 is comprised of two serpentine pathways, a first pathway 164 formed on the bottom of  
25 the first lamina 100 and a second pathway 264 formed on the top of the second lamina 200. The first and second pathways are each comprised of a series of straight segments and turning segments connected together to form a continuous path. The first and second pathways are  
30 positioned on abutting surfaces with the segments longitudinally offset such that the corresponding turning segments intersect repeatedly. The mixer element 64 (as illustrated by mixer element 64A2) may be described as having a double serpentine path (best seen  
35 in Figure 11).

Four pathways 160A, 160B, 160C and 160D, cooperate respectively with branches 40-1, 40-2, 40-3 of manifold 40, branches 44-1, 44-2, 44-3 of manifold 44 and a first straight segment 264S of each serpentine pathway 264 to form a series of T-mixers 62 (best seen in Figure 7). Each first straight segment 264S thus connects each T-mixer 62 with each serpentine mixer 64 of mixer array 60.

Figure 7 shows the arrangement of pathways that cooperate to form a collection manifold 50. As seen in Figures 6 and 7, collection manifold 50 is comprised of common chamber 50M and branch passages 50-1, 50-2, 50-3, 50-4, and 50-5. The vertical pathways 64A1V, 64A2V, 64A3V, 64A4V, and 64A5V connects the last segment of mixer 64A1, 64A2, 64A3, 64A4, 64A5 with the collection manifold branches 50-1, 50-2, 50-3, 50-4, and 50-5, respectively; the vertical pathway 64B1V, 64B2V, 64B3V, 64B4V, and 64B5V connects the last segment of mixer 64B1, 64B2, 64B3, 64B4, 64B5 with the collection manifold branches 50-1, 50-2, 50-3, 50-4, and 50-5, respectively; the vertical pathway 64C1V, 64C2V, 64C3V, 64C4V, and 64C5V connects the last segment of mixer 64C1, 64C2, 64C3, 64C4, 64C5 with the collection manifold branches 50-1, 50-2, 50-3, 50-4, and 50-5, respectively; and the vertical pathway 64D1V, 64D2V, 64D3V, 64D4V, and 64D5V connects the last segment of mixer 64D1, 64D2, 64D3, 64D4, 64D5 with the collection manifold branches 50-1, 50-2, 50-3, 50-4, and 50-5, respectively. Vertical passage 30V connects collection manifold 50 with the outlet port 30 on the first side of lamina 100. Vertical passage 34V connects manifold 50 with both outlet ports 34 on the first side of lamina 100 and the second side of the lamina 300, as best seen in Figure 5.

As best seen in Figure 8, each pathway 160 cooperates with manifolds 40 and 44 and a first straight segment of serpentine pathway 264 to form a T-mixer 62. This connects with a serpentine mixer 64, comprised of the multiple straight segments 264S and turning segments 264T. As also may be seen in Figure 8 each portion of pathway 160, e.g., portion 160A-1 between manifold 40-1 and segment 264S1 and portion 160A-2 between manifold 44-2 and segment 264S1, may be of a different cross-sectional size to provide the desired flow rate of each chemical being mixed. The number of straight and turning segments 164S, 164T and 264S, 264T and the cross-sectional size of each segment of 164 and 264 may be selected, according to the mixing requirements and flow characteristics of the chemicals being processed.

As seen in Figure 9 the serpentine pathways 164, 264 are comprised of straight segments designated with a suffix letter "S" (171S, 172S, 173S, 174S, 175S, and 271S, 272S, 273S, 274S, 275S) and turning segments designated with a suffix letter T (171T, 172T, 173T, 174T, 175T, and 271T, 272T, 273T, 274T, 275T). Corresponding turning segments (e.g., 171T, 271T) of pathways 164 and 264 intersect in a shearing fashion at a ninety (90) degree angle of attack. By slightly offsetting the position of pathway 164 relative to pathway 264 this angle of attack may be changed if desired. By rotating lamina 100 relative to lamina 200, and suitably altering the spacing of the straight segments (suffix S) and turning segments (suffix T), almost any desired angle of attack may be achieved. Angles of attack within the range of 20 degrees to 160 degrees may be readily realized, as is contemplated being within the scope of this invention.

Figure 10 shows an alternate arrangement of channels, which may be used in place of the arrangement

shown in Figures 6, 8, and 9. Figure 10 shows two channels 181, 182 in the bottom surface of lamina 100 that join at a point of intersection, traverse in a combined configuration as channel 183, are subsequently separated into two channels 184, 185, and then recombined as channel 186, separate into channels 187, 188. Channel 281 in the top surface of lamina 200 separates at a point of intersection into two channels 282, 283, which are then recombined as channel 284, are subsequently separated into two channels 285, 286, and then recombined as channel 287. Channel 181 intersects with channel 282 and channel 182 intersects with channel 283 at predetermined angles of attack and shear rates. Similarly channel 184 intersects with channel 282, channel 185 intersects with channel 283, channel 184 intersects with channel 286, channel 185 intersects with channel 287, channel 187 intersects with channel 286, channel 188 intersects with channel 287.

Figure 11 depicts the channels of Figure 9 in a somewhat simplified manner to better visualize the shape, relative position and intersections of the channels. As may be appreciated from Figures 9 and 11, two channels repeatedly intersect to form a double helix configuration, wherein a first channel 164 is comprised of straight segments and turning segments in a first plane, a second channel 264 is comprised of straight segments and turning segments in a second plane.

Chemicals within a first channel are repeatedly subjected to the sequence of: (a) a turbulent left hand turn, (b) a turbulent left hand shearing intersection with chemicals in a second channel, (c) a turbulent right hand turn, (d) a turbulent right hand turn, (e) a turbulent right hand shearing intersection with chemicals in the second channel, (f) a turbulent left hand turn.

Figure 12 depicts the channels of Figure 10 in a somewhat simplified manner to better visualize the shape, relative position and intersections of the channels. In this figure it can be seen that the two channels intersect at angles of attack and shear rates. Each channel comprises two or more channels that join at a point of intersection, traverse in a combined configuration, are subsequently separated into two or more channels, and then subsequently rejoin.

Figure 13(a)-(c) is a plan view of the channels of Figure 9. It shows channel 164 alone (Figure 13(c)), channel 264 alone (Figure 13(a)), and 164 superimposed with 264 (Figure 13(b)). At the point of intersection of the channels a centerline 164C of channel 164 and a centerline 264C of channel 264 are shown. The included angle  $\alpha$  between these centerlines is defined as the "angle of attack" of the two channels.

Multiple units of the chemical mixing and reaction apparatus can be used in sequence or in tandem. The incorporation of units in any number of sequential or tandem patterns is a design choice to be made by those skilled in the art and according to the desired chemical processing result.

As seen in Figures 9 and 10 the particular angles of the channel walls produced at the turning sections (e.g., 171T) are due to the orientation of the crystal planes of the silicon. In the illustrated example each lamina comprises a silicon wafer which has the major planar surface of the wafer in the {100} crystal plane. The sides of the straight segments (e.g. 171S, 271S) are aligned to be in the {110} crystal planes. When etched with an anisotropic etch, the major sides of the segments are bevelled from the vertical at a 57 degree angle and are in the {111} crystal planes. The outside corners between the straight segment 171S and the

turning segment 171T, are not sharp right angles but are beveled by two so-called beveling faceting planes, which are the {210} crystal planes, thus producing the bevelled corners which are best seen in Figures 9 and 10.

#### FABRICATION OF THE APPARATUS

The apparatus of the present invention is achieved by a multi-step fabrication process. First, a series of planar laminae or wafers, are processed to form desired patterns of pathways on one or both major surfaces of each lamina or through the thickness of the lamina. The laminae are then joined together to form a plurality of intersecting channels that accommodate the passage of chemicals.

In the preferred embodiment of the figures, the laminae are arranged and precisely oriented to locate the channels in adjacent laminae. These channels may be continuous or discontinuous along each of the laminae. Discontinuous channels are continuously aligned between adjacent laminae sufficient to form a continuous pathway therethrough. A typical channel is comprised of straight segments and turning segments in a first plane, straight segments and turning segments in a second plane and transition segments between the two planes. The straight or turning segments of a channel may be formed as a groove or trough entirely within one lamina. When assembled this groove cooperates with the facing planar surface of the adjacent lamina to close the cross-section of the channel. This is best illustrated by the cross-sectional view of distribution manifold 40 (seen as 40-1, 40-2, and 40-3) in Figure 4. Mirror image grooves or troughs on facing surfaces of adjacent laminae may cooperate to form a channel having a symmetrical cross-section. This is best illustrated by the cross-sectional view of collection manifold 50 (seen

as 50-1, 50-2, 50-3, 50-4, and 50-5) in Figur 4. Th  
transition segments of the channels may be passages that  
pass through a lamina to connect a channel segment on a  
first lamina with another segment on a second lamina or  
5 with a distribution or collection manifold. This is  
best illustrated by the cross-sectional view of vertical  
pathways 64A3V through 64D3V in Figure 5.

#### Processing of Laminae

The processing of the laminae to form pathways may  
10 be performed by a procedure selected from the group of:  
subtractive processes, additive processes, and forming  
processes. Subtractive processes comprise chemical  
etching, electrochemical machining (ECM), electrical  
discharge machining (EDM), laser ablation, drilling and  
15 cutting, abrasive grinding and single diamond point  
cutting (such as used to fabricate ceramic parts).  
Additive processes comprise deposition processes, such  
as electroforming, selective plating, chemical vapor  
deposition, stereo lithographic photoforming, and  
20 welding. Forming processes comprise molding, casting,  
and stamping. Wear resistant coatings, such as  
metalloid carbides, in the form of thin films, may be  
optionally deposited on the processed laminae before  
bonding.

#### 25 Materials of Construction

Selection of lamina materials is based upon the  
material's compatibility with the chemicals to be mixed  
and reacted. As used herein "compatibility with the  
chemicals to be mixed and reacted" includes without  
30 limitation: resistance to chemical degradation;  
operating conditions, such as temperature and pressure;  
thermal conduction requirements; required features to be  
created in the lamina, including size, geometrical shape  
and precision; the sealability of the lamina material;  
35 and economic considerations.

A variety of materials, may be used to construct the mixing/reaction units of the present invention. Crystalline materials that can be processed using photolithographic techniques may be used, especially  
5 when a mixing/reaction unit with extremely small cross-sectional passages are desired, for instance when gasses that react rapidly are to be processed. Such crystalline materials would typically include elements from groups III through V of the periodic table, for  
10 example silicon. Other compound materials, selected for their resistance to chemical attack, may be used to fabricate the laminae or may be used as coatings on the laminae. Ceramic materials may be used, such as silicon carbide, tungsten carbide, alumina and sapphire for  
15 instance using known molding, pressing and sintering techniques, to form the laminae. Thin films may be deposited on the surfaces of the laminae, such as by chemical vapor deposition techniques, to improve resistance of the passages to chemical attack or to  
20 facilitate bonding of the laminae. Glass materials, such as fused quartz, pure silica glass and borosilicate glass, as well as composite materials, such as ceramic composites and polymeric composites may be used.

For example, wafers similar to those used to  
25 fabricate semiconductor electronics components, such as single crystal silicon wafers, may be used. For such silicon wafers a combination of subtractive techniques may be used to form the passages. The laminae are subsequently stacked in precise alignment and joined  
30 together (as by bonding or clamping) into an integral structure. As illustrated in the example of Figure 1, three laminae are joined as an apparatus. The laminae may be of identical or different materials. The outer laminae may be silicon or a protective material such as  
35 metal, ceramic, composite material or glass while the

inner lamina would typically be silicon. If all the lamina are silicon, thermal fusion bonding is a preferred method of joining the laminae because the strength of the bond achieved approaches that of the laminae themselves.

#### OPERATION OF THE APPARATUS

Having reference to Figures 1-3, the two materials to be reacted flow into the unit through input ports 20, 24, through vertical passages 20V, 24V into distribution manifolds 40, 44 and into mixer array 60. Optional temperature control means (not shown) may be used to maintain the mixer array 60 at the desired temperature. The mixed material is collected in collection manifold 50 and passed through vertical passage 30V to the outlet port 30 or through vertical passage 34V to the outlet port 34.

Additional microfabricated process control elements, such as proportional valves, pressure, temperature and flow sensors, may be incorporated with the structure of the present invention. These elements, when used with external controls could regulate the flow of reactants within the integrated chemical processing unit and thus control the residence time. Any rapid chemical process, such as hydrolysis, nitration, polymerization, and oxidation may be practiced using the integrated structure of the present invention.

#### FABRICATION OF THE LAMINAE

In the preferred embodiment, most steps of the fabrication process generally correspond to known semiconductor processing techniques for silicon wafers. The photo-tools for the patterns for each side of each wafer are prepared using well known computer-aided-design techniques. Already polished silicon wafers, having the {100} crystal plane and other orientations on the major surfaces may be purchased from commercial

sources. The polished wafers are first cleaned using a well-known general cleaning technique, such as the "RCA process". An oxide film is grown on the wafer using well-known standard techniques. A nitride layer is  
5 deposited over the oxide layer using a known chemical vapor deposition method. The nitride layer protects the oxide layer from attack by the etch used to etch the silicon. A photoresist is applied, following the directions of the photo resist manufacturer, using the  
10 well-known spin coating technique.

The desired pattern is formed by first masking the wafer with a photo-tool having an image of the desired pattern, which is precisely aligned with the crystal planes of the wafer. Straight portions of the pattern  
15 are typically aligned along the {110} crystal plane. After exposing and developing the photoresist, the undeveloped photoresist is stripped to expose part of the nitride/oxide film layer. The exposed nitride/oxide film is finally etched to form an nitride/oxide film  
20 negative image of the desired pattern.

The pathways are formed in the surfaces of the wafers by etching the silicon, using either isotropic or anisotropic etch, the choice of which is dependent on the shape of the pathway desired. Curved shapes are  
25 etched using an isotropic etch. Straight shapes may employ either etch, depending on the desired cross-sectional shape pathway. If a trapezoidal cross-section is desired an anisotropic etch is used.

If a given wafer is to be etched on both major  
30 surfaces using the same etch, both sides of the wafer may be masked with resist, the resist exposed with the desired pattern on each surface, developed, washed and the nitride/oxide etched simultaneously on both surfaces. Then the silicon may be simultaneously etched  
35 on both surfaces. If different types of etchants are to

be used on each side of the wafer, all steps for the first etch are completed and then the steps are repeated for the second etch. After all the etching steps have been completed the vertical passages or vias through the wafer are formed by laser cutting through the wafers, typically using a pulsed neodymium-YAG laser cutting system. After laser cutting, the wafers are again recleaned to remove cutting debris. The remaining nitride layer of the negative image is removed from the wafer, by using a suitable solvent, such as boiling phosphoric acid, exposing the undamaged oxide layer. The remaining oxide layer negative image may optionally be removed from the wafer, by using a suitable solvent, such as buffered hydrogen fluoride. The wafer is recleaned, using the technique as described above.

Other techniques may be used which are dependent upon the lamina material. Laminae which are comprised of group III, IV or V material are processed using etching, grinding, drilling and polishing techniques. Laminae comprised of glass, Pyrex, or fused silica are fabricated using conventional glass cutting, drilling, grinding, and polishing techniques. Laminae comprised of ceramic materials may be formed by slip casting, consolidated by pressing and fired using well known techniques.

When all the laminae have been individually processed the laminae are carefully stacked in a precisely aligned manner and fusion bonded. To achieve good bonding of silicon laminae, the surfaces should be highly planar and the oxide layers on each surface should be undamaged. Since silicon is somewhat transparent in the infrared, a microscope with an infrared video camera may be used, with optional alignment indicia on each wafer, to insure precise alignment of the wafers before they are fusion bonded.

If an outer lamina is comprised of glass, this lamina is then anodically bonded to the already fused stack of inner laminae.

Those skilled in the art, having the benefit of the  
5 teachings of the present invention as hereinabove set forth, can effect numerous modifications thereto. It is readily appreciated that such modifications can be made without departing from the spirit of the scope of the present invention. Accordingly, such modifications are  
10 to be construed as being encompassed within the scope of the present invention as set forth in the appended claims.

CLAIMS

1. An apparatus for use in an integral structure for chemical mixing and reacting of one or more chemicals, comprising a plurality of laminae joined  
5 together and having a plurality of intersecting channels formed therethrough which accommodate the passage of one or more chemicals,  
said laminae comprising a material selected for compatibility with the one or more chemicals,  
10 said channels being formed so that chemicals are combined at intersections therein at sufficient angles of attack and shear rates so that chemical reactions are not limited by mass transfer considerations.
- 15 2. The apparatus of Claim 1 wherein the channels are generally planar, a first channel being disposed in a first plane and a second channel being disposed in a second plane, wherein the first and second planes are parallel and adjacent to each other, and the channels  
20 are generally serpentine and are offset from each other such that the first and second channels repeatedly intersect in a shearing fashion and form angles of attack at points of intersection.
3. The apparatus of Claim 2 wherein two or more  
25 channels are positioned at a point of intersection to form an angle of attack of 20 to 160 degrees.
4. The apparatus of Claim 3 wherein the angle of attack is 70-110 degrees.
5. The apparatus of Claim 3 wherein the angle of  
30 attack is 90 degrees.
6. The apparatus of Claim 1 wherein shear rate is sufficient to disrupt boundary layer formation.
7. The apparatus of Claim 1 wherein two or more  
35 channels intersect at aforesaid angles of attack and shear rates, each channel comprising two or more

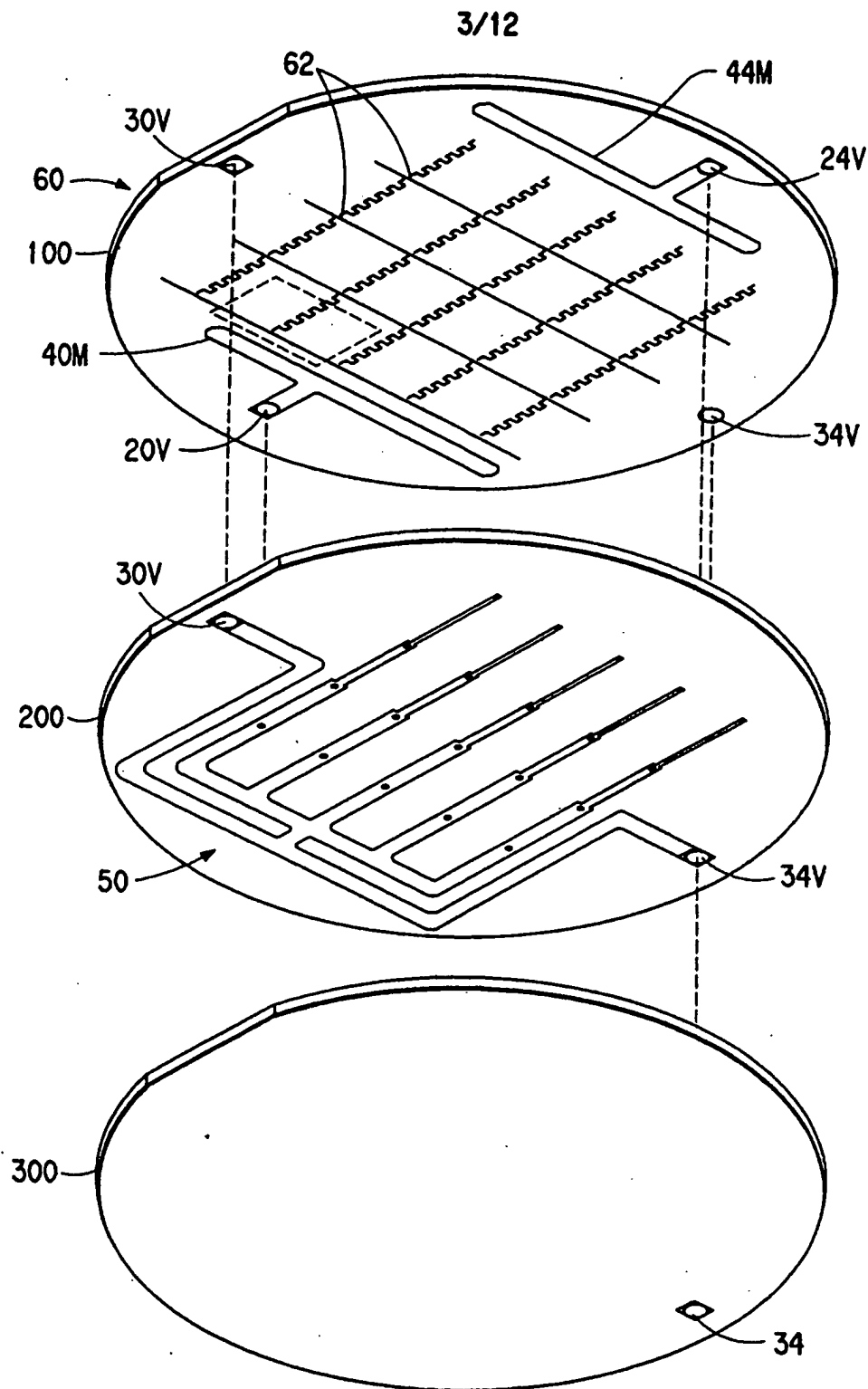


FIG. 3

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FIG. 4

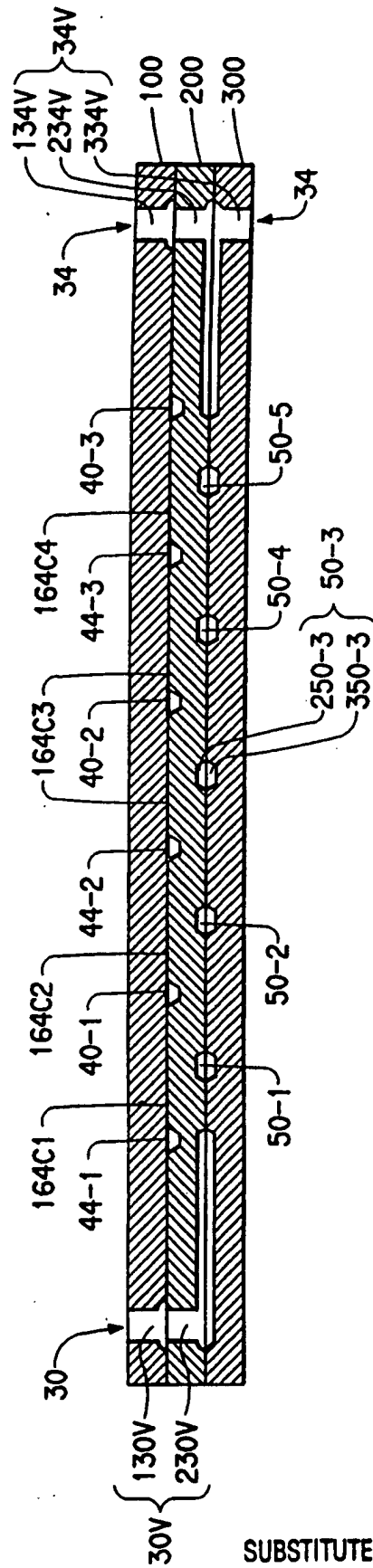
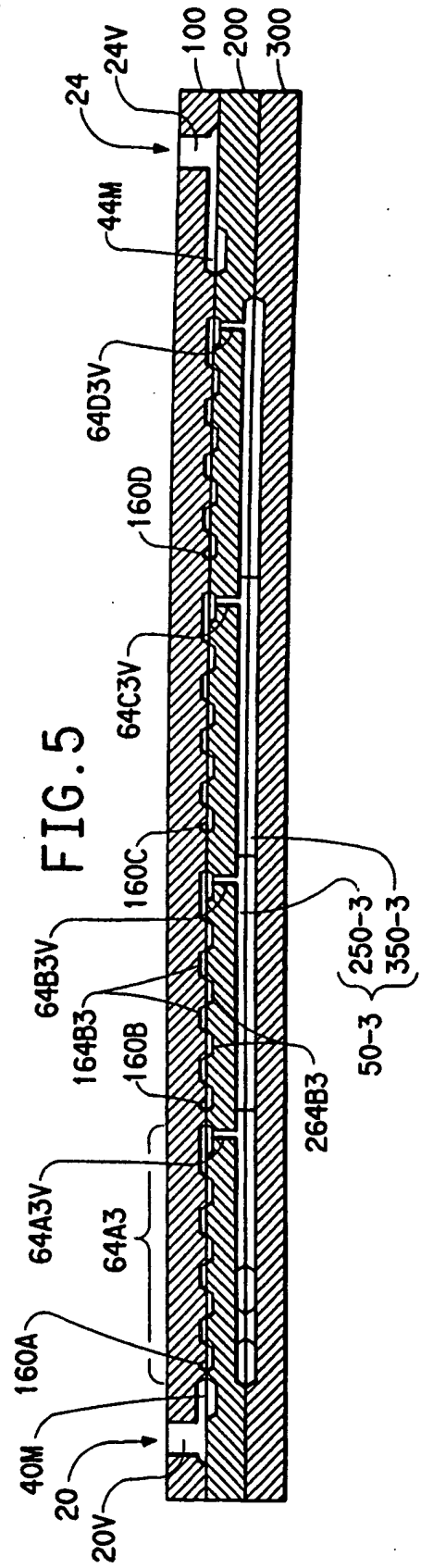


FIG. 5



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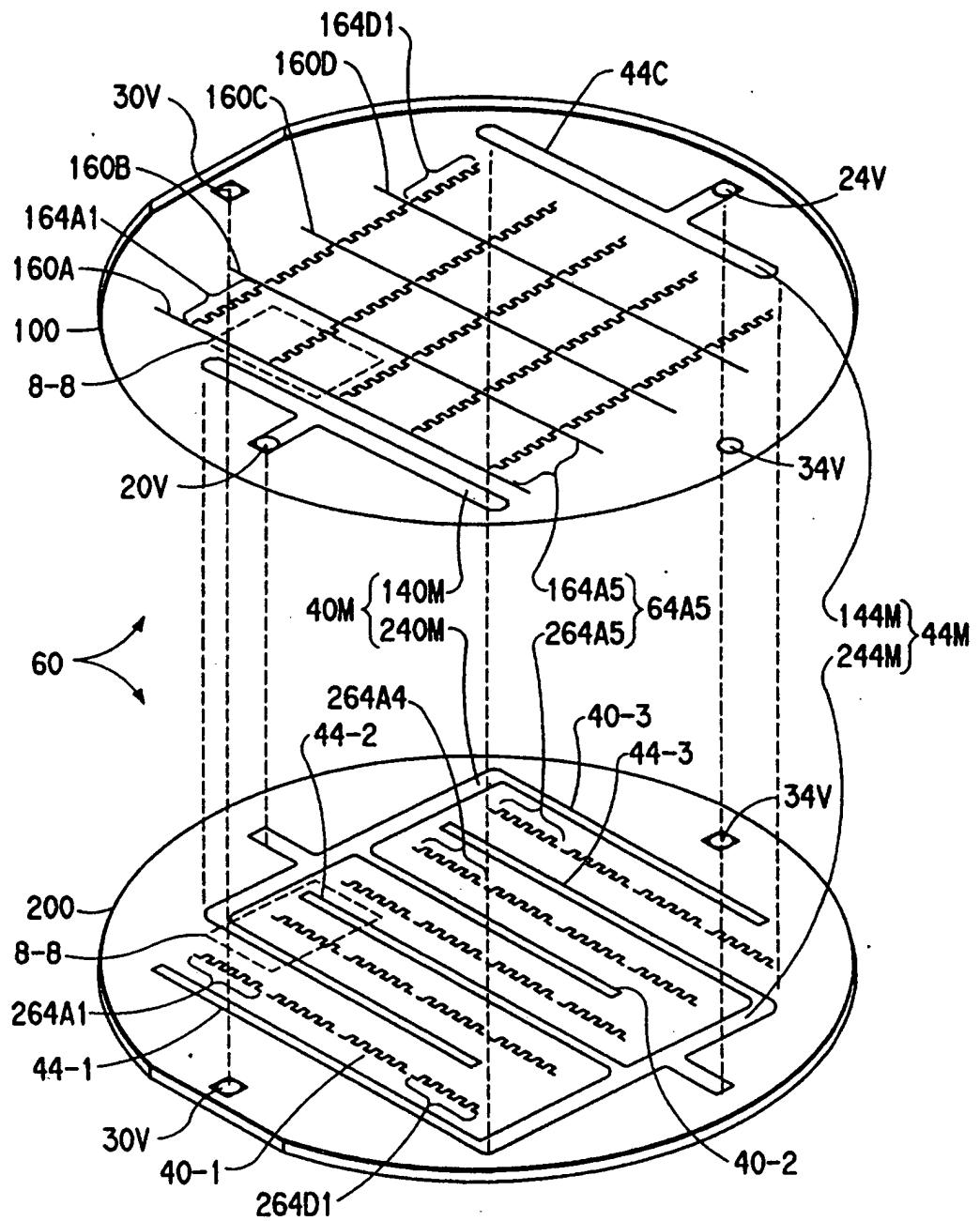


FIG. 6

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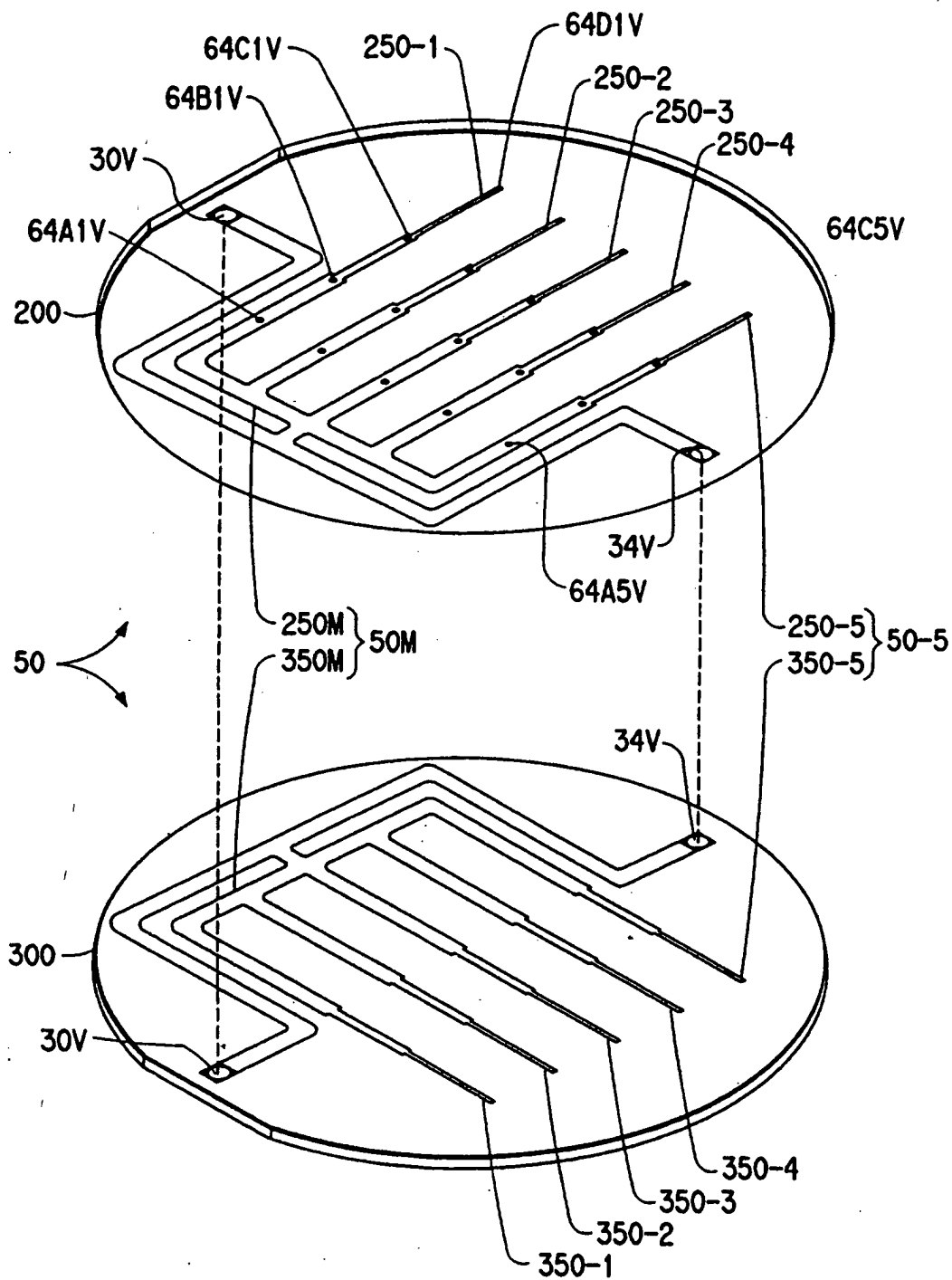


FIG. 7

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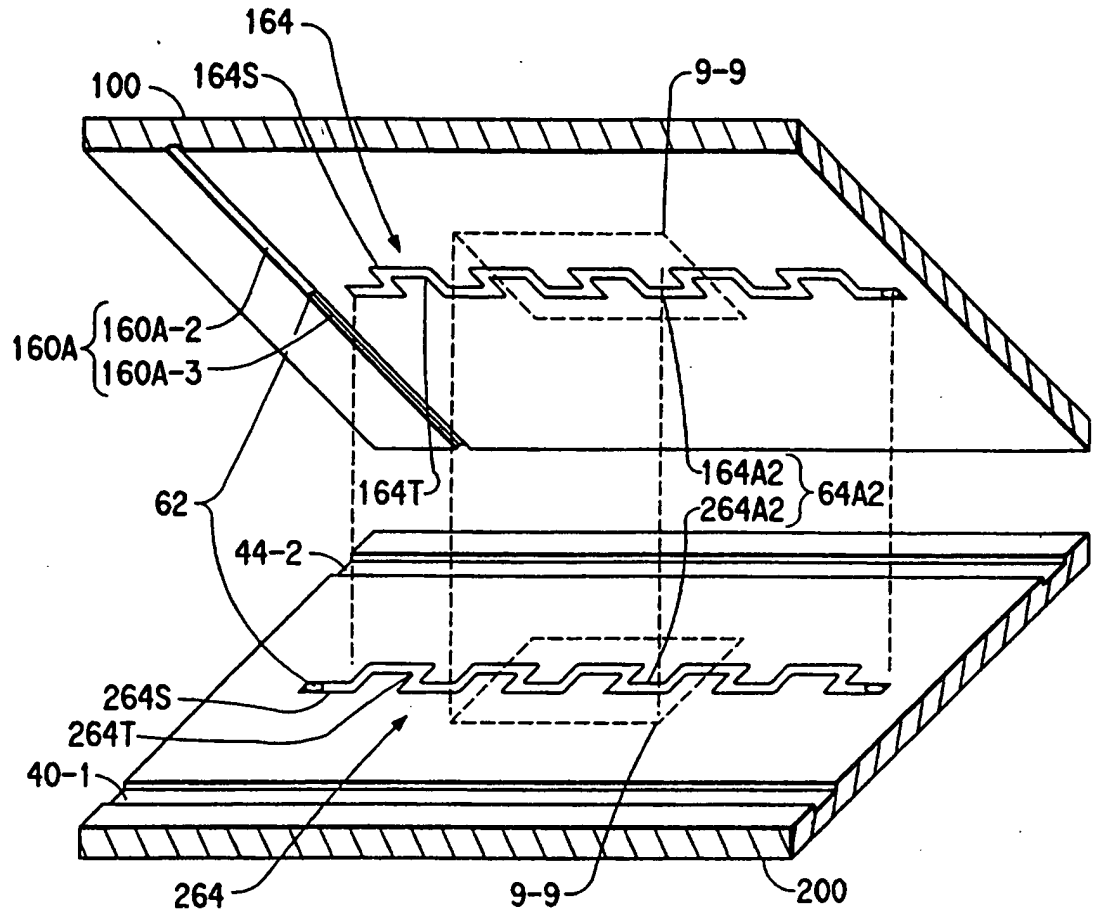


FIG. 8

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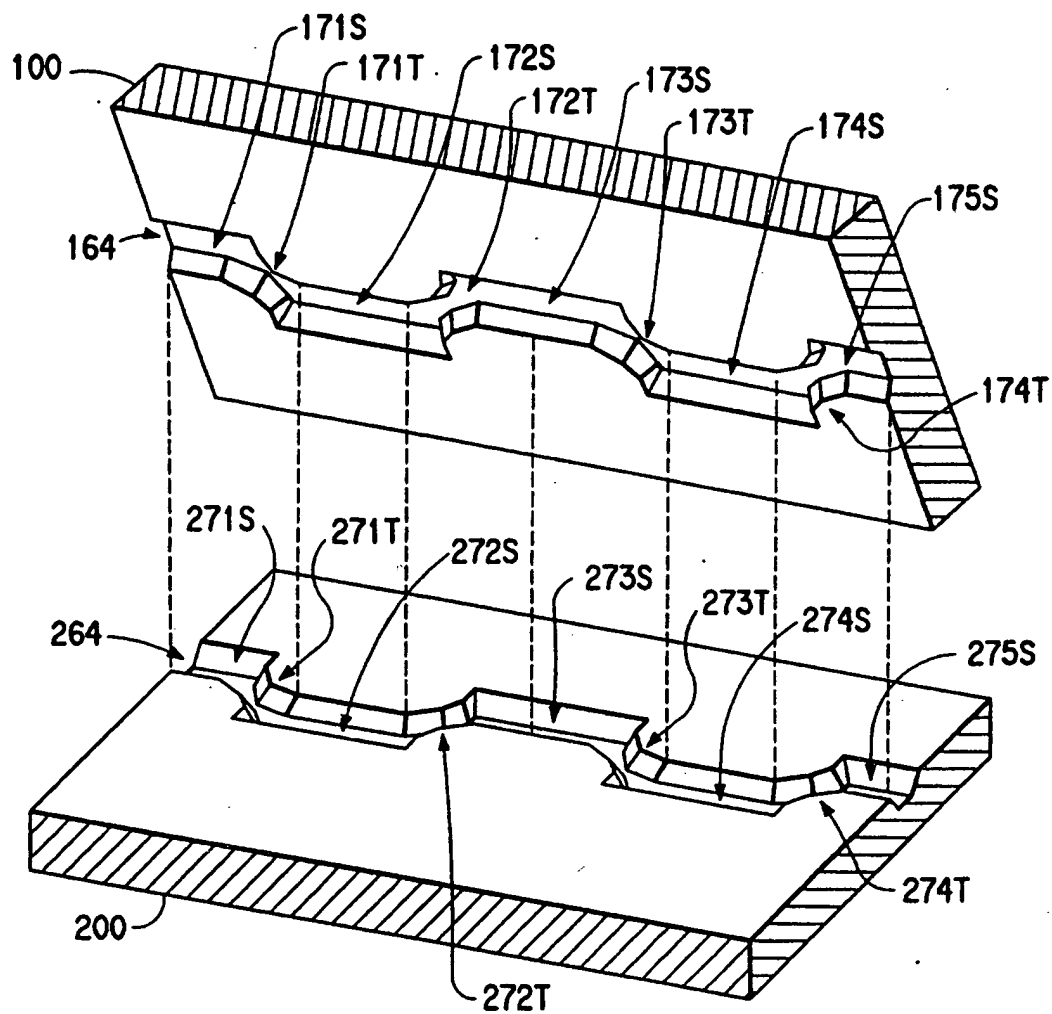


FIG. 9

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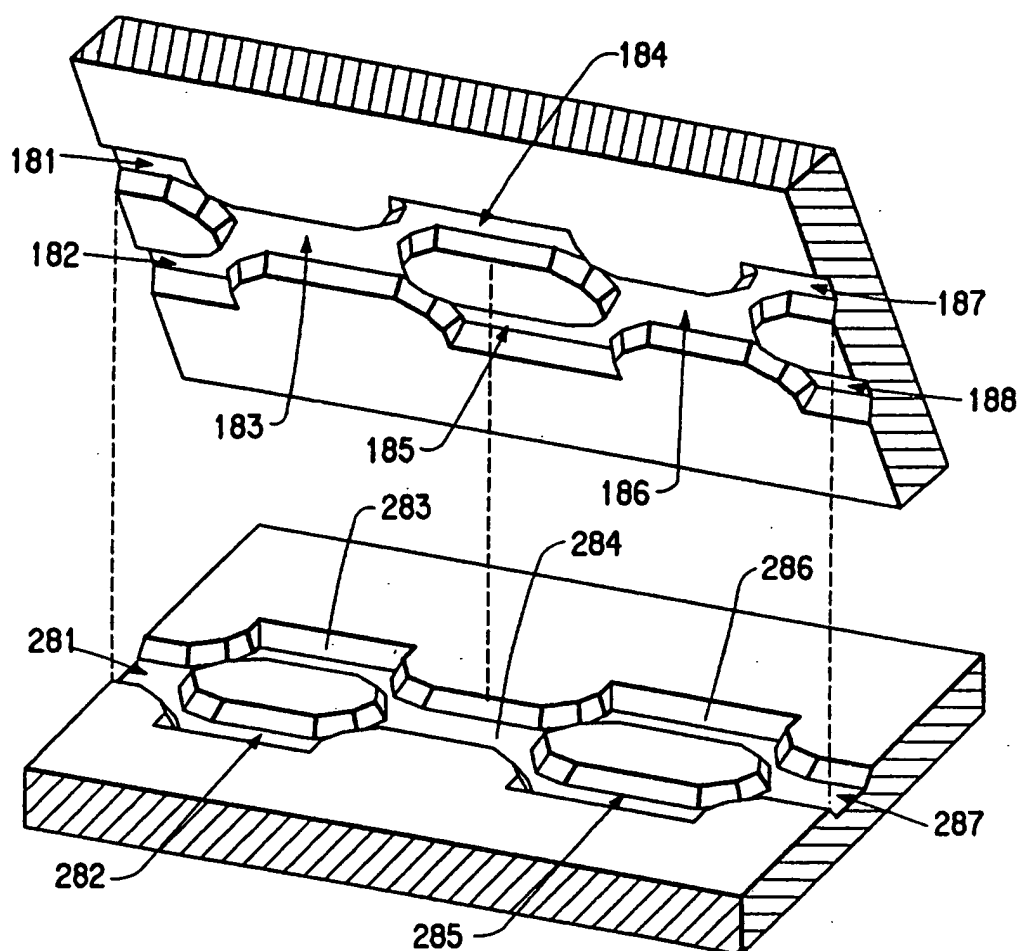


FIG. 10

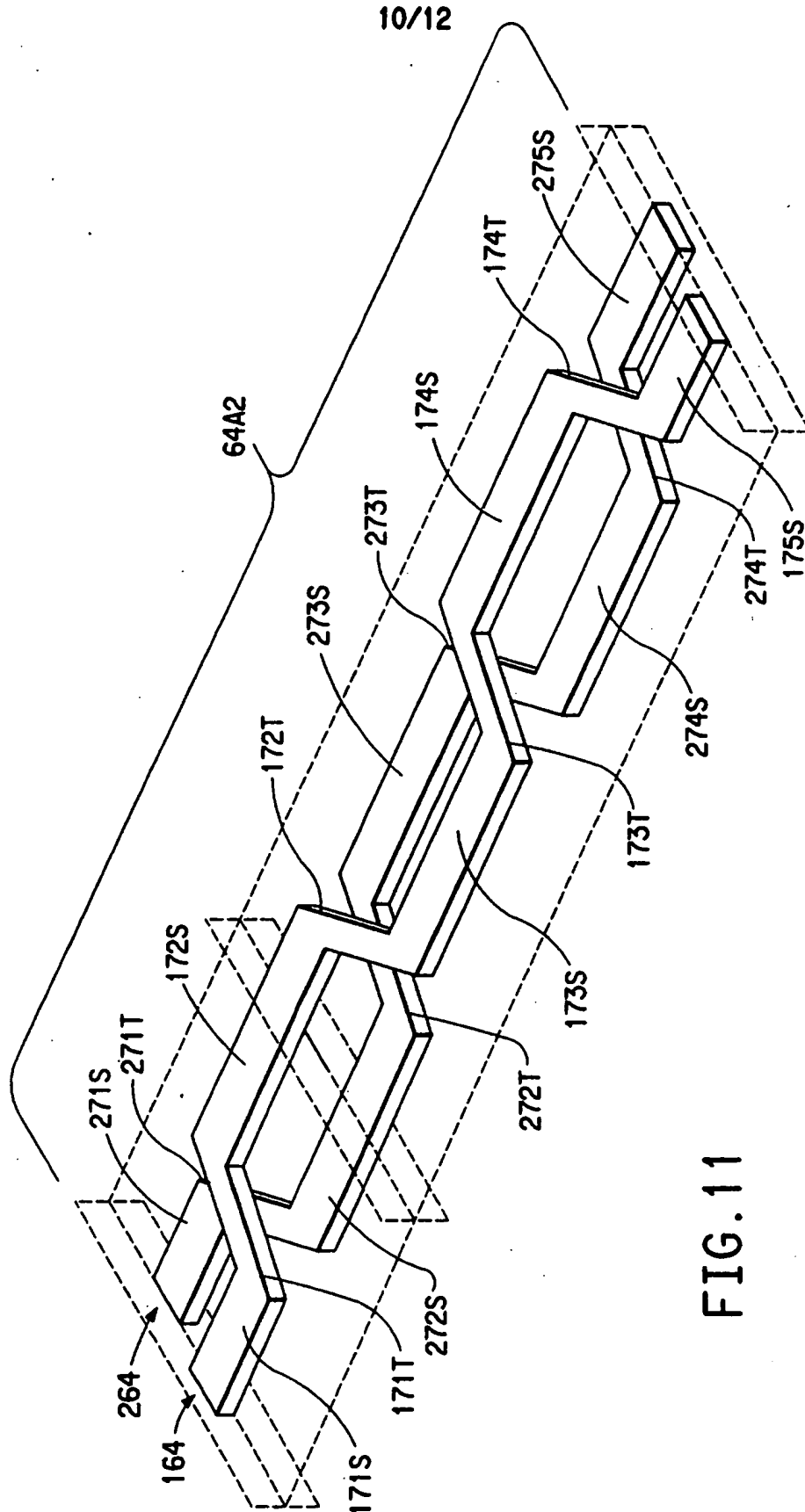


FIG. 11

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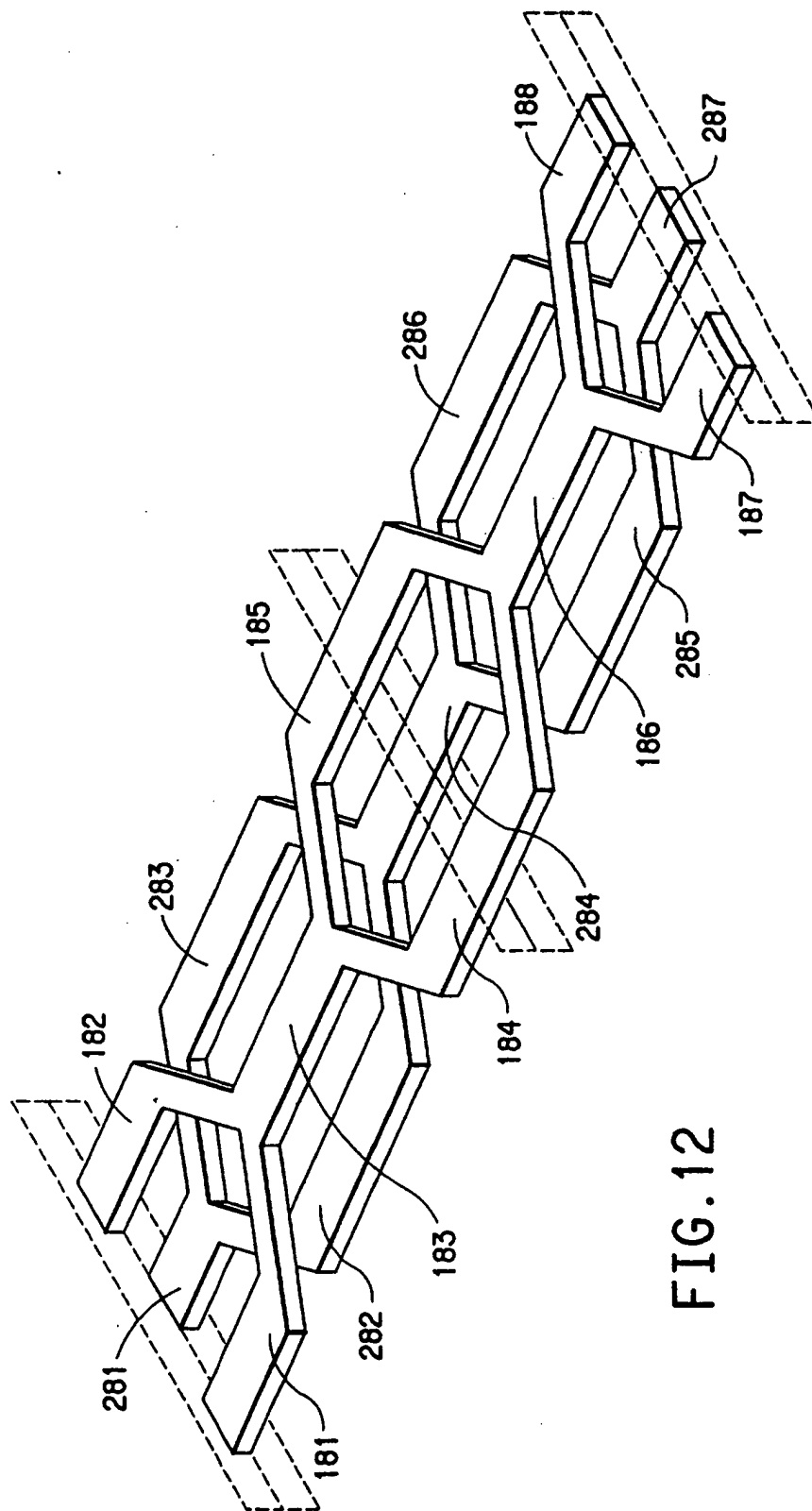


FIG. 12

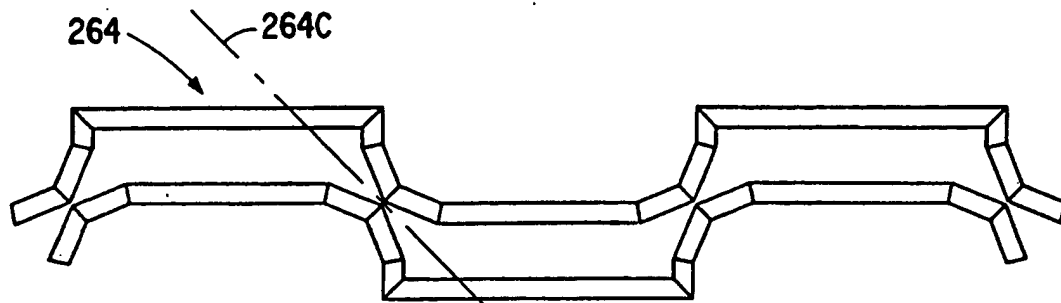


FIG. 13A

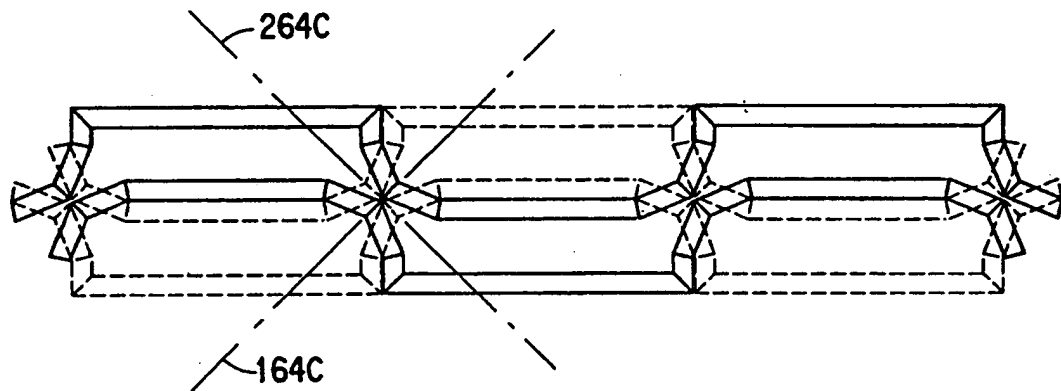


FIG. 13B

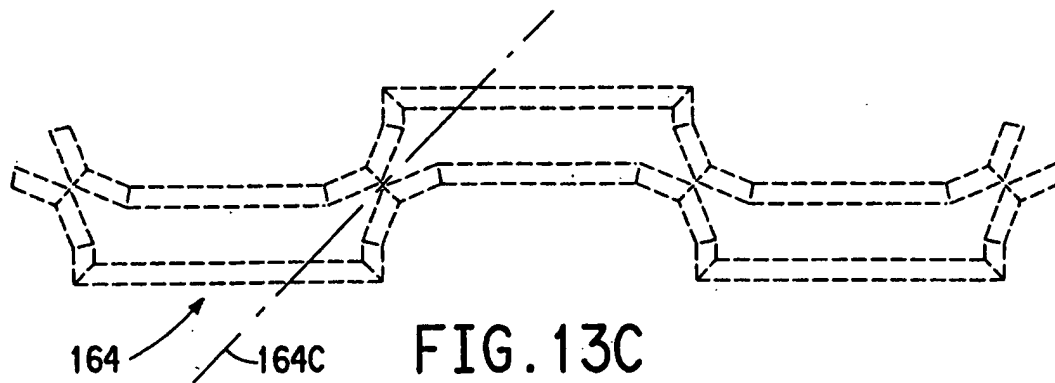


FIG. 13C

# INTERNATIONAL SEARCH REPORT

International Application No  
PCT/US 95/09834

## A. CLASSIFICATION OF SUBJECT MATTER

IPC 6 B01J19/00 B01F5/06 B01J12/00 B01J14/00 B01J19/12  
B01J35/04 B01L3/00

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 6 B01J B01F B01L

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US,A,5 252 294 (MESSERSCHMITT-BÖLKOW-BLOHM GMBH) 12 October 1993 see abstract see figures 1-9,15 see claims 1-8,15	1
A	FR,A,2 640 620 (INSTITUT FRANÇAIS DU PÉTROLE) 22 June 1990 see abstract see page 1, paragraph 1 see page 2, paragraph 2 - page 4, paragraph 2 see page 9, paragraph 5 - page 10, paragraph 3 see figures 1-3	1

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

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Date of the actual completion of the international search

27 November 1995

Date of mailing of the international search report

08.12.95

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# INTERNATIONAL SEARCH REPORT

International Application No  
PCT/US 95/09834

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
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A	DE,A,39 26 466 (MESSERSCHMITT-BÖLKOW-BLOHM GMBH) 14 February 1991 see abstract see column 1, line 26 - column 2, line 6 see column 2, line 23 - line 26 see figures 1,2 ---	1
A	US,A,3 856 270 (FMC CORPORATION) 24 December 1974 see abstract see figures 1-4 see column 3, line 8 - column 4, line 35 ---	1
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A	US,A,5 320 139 (MILLIPORE CORPORATION) 14 June 1994 see abstract see column 4, line 5 - column 7, line 29 see figures ---	1
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PCT/US 95/09834

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